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## UTILITY PATENT APPLICATION TRANSMITTAL

Attorney Docket No. B-1482 First Inventor or Application Identifier Yong Wang, et al.

steam reforming of a

(Only for new nonprovisional applications under 37 C.F.R. § 1.53(b), Express Mail Label No.

EJ017935648US

	ATION ELEMENTS concerning utility patent application contents.	Assistant Commissioner for Patents ADDRESS TO: Box Patent Application Washington, DC 20231
2. X Specification (preferred and preferred	smittal Form (e.g., PTO/SB/17) conginal and a duplicate for fee processing) on [Total Pages 8] rrangement set forth below) we title of the Invention ferences to Related Applications at Regarding Fed sponsored R & D e to Microfiche Appendix	5 Microfiche Computer Program (Appendix) 6. Nucleotide and/or Amino Acid Sequence Submission (if applicable, all necessary) a. Computer Readable Copy b. Paper Copy (identical to computer copy) c. Statement verifying identity of above copies
l	and of the Invention	ACCOMPANYING APPLICATION PARTS
- Brief Surn - Brief Desc - Detailed [ - Claim(s) - Abstract of the continuation of th	mary of the Invention cription of the Drawings (if filed) Description  of the Disclosure  (35 U.S.C. 113) [Total Sheets 1]  ion [Total Pages 3]  why executed (original or copy)  py from a prior application (37 C.F.R. § 1.63(**) recontinuation/divisional with Box 16 completed)  DELETION OF INVENTOR(S) Signed statement attached deleting inventor(s) named in the prior application see 37 C.F.R. §§ 1.63(d)(2) and 1.33(b).  13: IN ORDER TO BE ENTITLED TO PAY SMALL ENTITY OF APPLICATION IS RELIED UPON (37 C.F.R. § 1.27), EXCEPT OR APPLICATION IS RELIED UPON (37 C.F.R. § 1.28).  NG APPLICATION, check appropriate box, and in Divisional Continuation-in-part (information: Examiner or DIVISIONAL APPS only: The entire disclosure	7. X Assignment Papers (cover sheet & document(s))  8. 37 C.F.R.§3.73(b) Statement Power of Attorney  9. English Translation Document (if applicable)  10. Information Disclosure Copies of IDS Statement (IDS)/PTO-1449 Citations  11. Preliminary Amendment  12. X Return Receipt Postcard (MPEP 503) (Should be specifically itemized)  13. X Small Entity Statement filed in prior application Status still proper and desired (PTO/SB/09-12)  14. Certified Copy of Priority Document(s) (if foreign priority is claimed)  15. Other:
reference. The incorp	poration can only be relied upon when a portion  17. CORRESPOND	has been inadvertently omitted from the submitted application parts.
Customer Numb	er or Bar Code Label (Insert Customer No. or At	or 🔯 Correspondence address below
	<u>  W. Zimmerman (K1-53)</u> telle Memorial Institute	
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## IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re Application of:
Y Wang, DP Vanderwiel, AY Tonkovich

For: A METHOD FOR STEAM REFORMING

OF A HYDROCARBON

Our Ref. No: B-1482

Date: August 17, 1999

CERTIFICATE OF MAILING

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PATENT

File No. B-1482

## IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Applicant or Patentee: <u>Yong Wang, David P. Vanderwiel, Anna Lee Y. Tonkovich</u>
Serial or Patent No.:
Filed or Issued:
For: A METHOD FOR STEAM REFORMING OF A HYDROCARBON
VERIFIED STATEMENT (DECLARATION) CLAIMING SMALL ENTITY STATUS (37 CFR 1.9(f) and 1.27(d)) - NONPROFIT ORGANIZATION
I hereby declare that I am an official empowered to act on behalf of the nonprofit organization identified below:
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ADDRESS OF ORGANIZATION Post Office Box 999, Richland, WA 99352
TYPE OF ORGANIZATION:
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I hereby declare that the nonprofit organization identified above qualifies as a nonprofit organization as defined in 37 CFR 1.9(e) for purposes of paying reduced fees under section 41(a) and (b) of Title 35, United States Code with regard to the invention entitled <u>A METHOD FOR STEAM REFORMING OF A HYDROCARBON</u> by inventor(s) Yong Wang, David P. Vanderwiel, Anna Lee Y. Tonkovich described in
<pre>[ ] application executed [X] specification filed herewith [ ] application serial no, filed</pre> <pre>[ ] patent no, issued</pre>

I hereby declare that rights under contract or law have been conveyed to and remain with the nonprofit organization with regard to the above identified invention.

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\*NOTE: Separate verified statements are required from each named person, concern or organization having rights to the invention averring to their status as small entities. (37 CFR 1.27)

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I acknowledge the duty to file, in this application or patent, notification of any change in status resulting in loss of entitlement to small entity status prior to paying, or at the time of paying, the earliest of the issue fee or any maintenance fee due after the date on which status as a small entity is no longer appropriate.  $(37\ \text{CFR } 1.28(b))$ 

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NAME OF PERSON SIGNING <u>Paul W. Zimmerman</u>
TITLE OF ORGANIZATION <u>Contracting Officer, Pacific Northwest Division</u> ,
Battelle Memorial Institute
ADDRESS OF PERSON SIGNING Post Office Box 999, Richland, WA 99352

SIGNATURE <u>Paul M. Simmorman</u> DATE <u>99/AV6/17</u>

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## A METHOD AND CATALYST STRUCTURE FOR STEAM REFORMING OF A HYDROCARBON

#### FIELD OF THE INVENTION

The present invention is a method and catalyst structure for steam reforming of a hydrocarbon.

#### BACKGROUND OF THE INVENTION

Steam reforming of hydrocarbons is commonly used for feedstock production for carbon-monoxide hydrogenation (Fischer-Tropsch synthesis), methanol synthesis and hydrogen production. Steam reforming is done commercially by flowing a mixture of steam and the hydrocarbon past a supported catalyst having an alumina support and a catalyst metal thereon, and reacting the mixture at a temperature from about 600 °C to about 1000 °C, forming at least one product. Research has been done with the catalyst metal on a spinel support. Residence times are typically on the order of seconds and steam tocarbon ratio greater than about 2.5. For steam to carbon ratio less than 2.5, catalyst activity is generally degraded after hours to days due to coke formation and the supported catalyst must be refreshed or replaced.

The rate of supported catalyst activity degradation has been reduced by use of excess steam (steam to carbon ratio greater than 2.5). Excess steam, however, requires excess thermal energy and results in large system pressure drop. Using less steam results in faster degradation of catalyst activity because of coking from the hydrocarbon(s).

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Hence, there is a need for a method of steam reforming of a hydrocarbon that provides greater product yield and permits using less steam and maintaining catalytic activity of the catalyst.

#### SUMMARY OF THE INVENTION

The present invention includes an improvement to the existing method of steam reforming of hydrocarbon, wherein the improvement comprises:

the flowing is at a rate providing a residence time less than about 0.1 sec resulting in obtaining product formation yield or amount that is the same or greater compared to product formation at a longer residence time.

Another improvement of the present invention is operation at a steam to carbon ratio that is substantially stoichiometric and maintaining activity of the supported catalyst.

The present invention also includes a catalyst structure for steam reforming of a hydrocarbon. The catalyst structure has

- (a) a first porous structure with a first pore surface area and a first pore size of at least about 0.1  $\mu m$ ;
- (b) a porous interfacial layer that is a spinel with a second pore surface area and a second pore size less than the first pore size, the porous interfacial layer having a thickness less than 4 mm placed upon the first pore surface area;
- (c) a steam reforming catalyst selected from the group consisting of rhodium, iridium, nickel, palladium, platinum, carbide of group VIb and combinations thereof placed upon the second pore surface area.

It is an object of the present invention to provide a method of steam reforming of hydrogen with a residence time of less than about 0.1 sec.

It is an object of the present invention to provide a catalyst structure with a porous interfacial layer of spinel.

The subject matter of the present invention is particularly pointed out and distinctly claimed in the concluding portion of this specification. However, both

the organization and method of operation, together with further advantages and objects thereof, may best be understood by reference to the following description taken in connection with accompanying drawings wherein like reference characters refer to like elements.

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#### BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a graph of conversion and selectivity versus temperature.

FIG. 2 is a graph of conversion and selectivity versus time.

## DESCRIPTION OF THE PREFERRED EMBODIMENT(S)

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The present invention includes a method for steam reforming of a hydrocarbon having the steps of flowing a mixture of steam and the hydrocarbon past a supported catalyst having a support and a catalyst metal thereon. The mixture is reacted at a temperature from about 600 °C to about 1000 °C forming at least one product. The improvement of the present invention is using a spinel support and flowing the mixture at a rate providing a residence time less than about 0.1 sec and obtaining product formation that is the same or greater than that obtained at longer residence times.

Also, under the previously described conditions, catalytic activity is degraded when the steam to carbon ratio is substantially stoichiometric. Another improvement of the present invention realized by flowing the mixture at a rate providing a residence time less than about 0.1 sec is maintaining activity of the spinel supported catalyst beyond 6 hours without degradation by coking even for substantially stoichiometric steam to carbon ratio. Substantially stoiciometric is a steam to carbon content ratio greater than about 0.9 and less than about 2.5, preferably from about 0.98 to about 2.

The supported catalyst may be in the form of a powder of non-porous particles, porous solid and combinations thereof.

Hydrocarbon includes oxygenates, alkanes, alkenes, alkynes, branched isomers, aromatics, saturated and unsaturated hydrocarbons and combinations thereof including fuels such as gasoline, kerosine, diesel, JP-8.

## 5 Example 1

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An experiment was conducted to demonstrate the present invention. The supported catalyst was spinel of a gamma-alumina ( $\gamma$ -Al<sub>2</sub>O<sub>3</sub>) support with a magnesia (MgO) passivation layer and rhodium oxide (Rh<sub>2</sub>O<sub>3</sub>). The approximate composition was about 15 wt% Rh<sub>2</sub>O<sub>3</sub>, about 5 wt% MgO, and about 80 wt%  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. The supported catalyst was prepared by (1) calcining a high surface area  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> at 500 °C for 5 hours; (2) impregnating the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> with MgO using the incipient wetness technique with a solution of magnesium nitrate; and obtaining an MgO modified  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> support; (3) drying the modified support at 110 °C for 4 hours followed by (4) a second calcination at 900 °C for 2 hours; (5) impregnating the modified support with Rh<sub>2</sub>O<sub>3</sub> with the incipent wetness technique from a rhodium nitrate solution; (6) followed by a final drying 110 °C for 4 hours and a (7) a final calcination at 500 °C for 3 hours to obtain a powder of the supported catalyst.

A microreactor was constructed of a quartz tube with 4mm ID and 6.35 mm OD. About 0.2 g of powder of supported catalyst was placed in the microreactor in a packed bed arrangement.

Reactants were steam and methane in a steam to carbon ratio of approximately 1 which is stoichiometric within measurement uncertainty.

Reactants were flowed through the reactor at temperatures from 650 °C to 900 °C.

Results are shown in **FIG. 1** for a steam to carbon ratio of 3 with conversion ranging from about 52% to 95% with increasing temperature and selectivity ranging from 22% to 70%.

Results in **FIG. 2** are for a steam to carbon ratio of 1 at 900 °C over 40 hours. No degradation of the supported catalyst was observed. Electron microscopic examination after testing revealed no coke deposition and BET measurements detected no significant loss in surface area.

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#### **CLOSURE**

While a preferred embodiment of the present invention has been shown and described, it will be apparent to those skilled in the art that many changes and modifications may be made without departing from the invention in its broader aspects. The appended claims are therefore intended to cover all such changes and modifications as fall within the true spirit and scope of the invention.

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1. A method for steam reforming of a hydrocarbon having the steps of flowing a mixture of steam and said hydrocarbon past a supported catalyst having a support and a catalyst metal thereon, and reacting said mixture at a temperature from about 600 °C to about 1000 °C forming at least one product; wherein the improvement comprises:

said support is a spinel support; and

said flowing is at a rate providing a residence time less than about 0.1 sec and obtaining said forming the same or greater compared to said forming at a longer residence time.

- 2. The method as recited in claim 1, wherein said mixture has a steam to carbon ratio less than 2.5, said improvement maintaining activity of said supported catalyst beyond 6 hours.
- 3. The method as recited in claim 1, wherein said spinel support controls acidity of said supported catalyst.
- 4. A method for steam reforming of a hydrocarbon having the steps of flowing a mixture of steam and said hydrocarbon having a steam to carbon ratio that is substantially stoichiometric past a supported catalyst having a support and a catalyst metal thereon, and reacting said mixture at a temperature from about 600 °C to about 1000 °C forming at least one product and degrading catalytic activity of said supported catalyst; wherein the improvement comprises:

said support is a spinel support; and

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said flowing is at a rate providing a residence time less than about 0.1 sec and maintaining activity of said supported catalyst for said steam to carbon ratio less than 2.5.

- 5. The method as recited in claim 4, wherein said support is spinel that controls acidity of said supported catalyst.
  - 6. The method as recited in claim 4, wherein said steam to carbon ratio is greater than about 0.9 and less than about 2.5.
- 7. The method as recited in claim 4, wherein said supported catalyst is on a porous substrate.
  - 8. A catalyst structure for steam reforming of a hydrocarbon, comprising:
  - (a) a first porous structure with a first pore surface area and a first pore size of at least about 0.1  $\mu$ m;
    - (b) a buffer layer upon said first pore surface area;
  - (c) a porous interfacial layer that is a spinel with a second pore surface area and a second pore size less than said first pore size, said porous interfacial layer having a thickness less than 4 mm placed upon said buffer layer;
  - (d) a steam reforming catalyst selected from the group consisting of rhodium, iridium, nickel, palladium, platinum, carbide of group IVb and combinations thereof placed upon said second pore surface area.
  - 9. The catalyst structure as recited in claim 8, wherein said carbide is selected from the group of tungsten carbide, molybdenum carbide and combinations thereof.

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#### **ABSTRACT**

The present invention includes an improvement to the existing method of steam reforming of hydrocarbon, wherein the improvement comprises: the flowing is at a rate providing a residence time less than about 0.1 sec resulting in obtaining product formation yield or amount that is the same or greater compared to product formation at a longer residence time. Another improvement of the present invention is operation at a steam to carbon ratio that is substantially stoichiometric and maintaining activity of the supported catalyst. The present invention also includes a catalyst structure for steam reforming of a hydrocarbon.

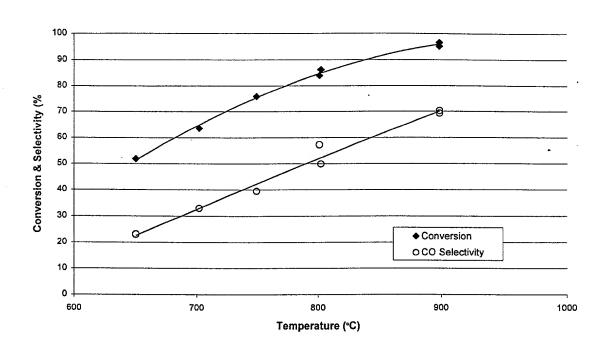


Figure 1. Steam reforming of methane over Rh/MgO/Al<sub>2</sub>O<sub>3</sub> (25-msec, H<sub>2</sub>O:CH<sub>4</sub> = 3:1)

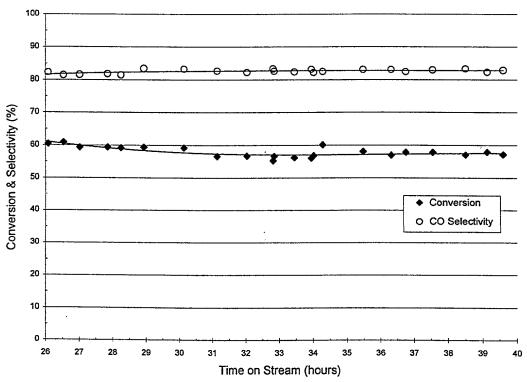


Figure 2. Steam reforming of methane over Rh/MgO/Al<sub>2</sub>O<sub>3</sub> (25-msec, H<sub>2</sub>O:CH<sub>4</sub> = 1:1, 900°C)

# COMBINED DECLARATION AND POWER OF ATTORNEY FOR PATENT APPLICATION

As a below named inventor, I hereby declare that:

My residence, post office address, and citizenship are as stated below next to my name,

I believe I am an original, first, and joint inventor of the subject matter which is claimed and for which a patent is sought on the invention entitled A METHOD FOR STEAM REFORMING OF A HYDROCARBON, the specification of which

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[] and was amended on(if applicable)	
[] with amendments through (if applicable)	
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[X] no such applications have been filed	
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Prior Forei	gn Application(s)		Prio Clai	
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(Number)	(Country)	(Day/Month/Year Filed)	L J Yes	[] No
		r Title 35, United States (		Sec.

I hereby claim the benefit under Title 35, United States Code, Sec. 120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, Sec. 112, I acknowledge the duty to disclose material information as defined in Title 37, Code of Federal Regulations, Sec. 1.56(a) which occurred between the filing date of the prior application and the national or PCT international filing date of this application:

#### NONE

(Application Serial No.)	(Filing Date)	(Status - patented, pending, abandoned)
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I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application, to file a corresponding international application, and to transact all business in the Patent and Trademark Office connected therewith:

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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

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Inventor's signature and Lee 4. Tonkor 8-17-99 Date
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